# Hydrogen production in DBD reactor powered with nanosecond high voltage pulses

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Balatonalmádi, 25-29 August 2013

Nanosecond voltage pulses much more efficient in H<sub>2</sub> production than AC



### $\square$ H<sub>2</sub>O inhibits H<sub>2</sub> production





5<sup>th</sup> CESPC, Balatonalmádi, 25-29 August 2013



GC-TCD, FTIR

- Quartz glass tube: inner diameter 15 mm
- RVC (Reticulated Vitreous Carbon) electrode:
  - outer diameter 8 mm,
  - inner diameter 3 mm,
  - length 150 mm,
  - low porosity 80 ppi (pores per inch),
- Gas composition and flow rate:
  - $CH_4:CO_2:H_2S = 69\%:30\%:1\%$
  - 200 cm<sup>3</sup>/min.

- Power supply:
  - Pulse generator NPG-15/2000 by Megaimpulse Ltd.
  - -29 kV, 50 Hz 3 kHz





### **DBD reactors** RVC electrode and porous ceramic tube



- Quartz glass tube: inner diameter 15 mm
- RVC (Reticulated Vitreous Carbon) electrode in porous ceramic tube:
  - outer diameter 12 mm,
  - inner diameter 8 mm,
  - length 150 mm
- Gas composition and flow rate:
  - $CH_4:CO_2:H_2S = 69\%:30\%:1\%$
  - 200 cm<sup>3</sup>/min.

- Power supply:
  - Pulse generator NPG-15/2000 by Megaimpulse Ltd.
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### **DBD reactors** RVC electrode and porous ceramic tube and Ni



- Quartz glass tube: inner diameter 15 mm
- RVC (Reticulated Vitreous Carbon) electrode in porous ceramic tube:
  - outer diameter 12 mm,
  - inner diameter 8 mm,
  - length 150 mm,
  - saturated with Ni
- Gas composition and flow rate:
  - CH<sub>4</sub>:CO<sub>2</sub>:H<sub>2</sub>S = 69%:30%:1%
  - 200 cm<sup>3</sup>/min.

- Power supply:
  - Pulse generator NPG-15/2000 by Megaimpulse Ltd.
  - -29 kV, 50 Hz 3 kHz







GC-TCD, FTIR

- Quartz glass tube: inner diameter 15 mm
- RVC electrode and glass beads Ø3 mm:
- Gas composition and flow rate:
  - CH<sub>4</sub>:CO<sub>2</sub> = 70%:30%
  - 200 cm<sup>3</sup>/min.

- Power supply:
  - Pulse generator NPG-15/2000 by Megaimpulse Ltd.
  - -29 kV, 50 Hz 3 kHz





# **Results** H<sub>2</sub> and CO production





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Thermodynamic Equilibrium Reactor, no ions, no electrons

### Close to thermodynamic equilibrium





# **Results** $H_2$ and CO production – $H_2$ S influence





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# **Results** $H_2$ and CO production – $H_2$ S influence





### **Results** C2 and C3 by-products





Ni catalyst activated due to heating the ceramic barrier





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- □ H<sub>2</sub>S increases C<sub>2</sub>H<sub>2</sub> formation





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- Ni catalyst activated due to heating the ceramic barrier
- H<sub>2</sub>S increases C<sub>2</sub>H<sub>2</sub> formation
- $\Box$  H<sub>2</sub>S (or sulfur) poisons the Ni catalyst





### **Results** C2 and C3 by-products





### **Results** CH<sub>4</sub> conversion and selectivity





**Results** H<sub>2</sub>S

 $H_2S = H_2 + S$ 





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**Results** 





### **Results** OES – influence of $H_2S$





### Results Packed bed DBD reactor



### Reactor with RVC and glass beads = Reactor with RVC only



Reactor with RVC and glass beads  $\approx$  Reactor with RVC only





# Conclusions

- Influence of reactor geometry:
  - higher H<sub>2</sub> production in the DBD with RVC only due to the higher discharge energy,
  - different by-products profile:
    - $\circ$  C2 hydrocarbons  $\checkmark$  when discharge energy 7,
    - $\circ$  C3 hydrocarbons **7** when discharge energy **7**,
- Influence of Ni catalyst:
  - activated at higher pulse repetition rate,
  - decreases C<sub>2</sub>H<sub>2</sub> production,
- $\Box \quad Influence of H_2S:$ 
  - is converted into soil sulfur directly and via CS<sub>2</sub>,
  - changes discharge parameters due to deposited sulfur,
  - decreases CH<sub>4</sub> conversion and H<sub>2</sub> production,
  - poisons Ni catalyst (no activation observed).

### Thank you for your attention!